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2010/04/05
2010/09/27

η_c

γ_c

$(n < 1)$

B

(Barus)

L/R

.B

Studying the flow behavior of white Vaseline "which is used in pharmaceutical industry and Cosmetics" in statical state

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Received 05/04/2010

Accepted 27/09/2010

ABSTRACT

The aim of this work is to study the flow behavior of white Vaseline "which is used in pharmaceutical industry and Cosmetics" in statical state.

The study was carried out on the white vaseline in the molten state under the effect of temperture, shear stress (τ), and shear rate ($\dot{\gamma}$) by using capillary viscometer, then the corrections have been done to expermental data. It was found from the obtained results that, real viscosity decreased with increasing real shear rate ($\dot{\gamma}_c$). Also it was found that the vaseline is a pseudoplastic material ($n < 1$).

For determining viscous activation energy at constant shear rtae ($E\dot{\gamma}$) and shear stress ($E\tau$), the relationship between real viscosity (η_c) and ($1/T$) was studied. It was found that the viscous activation energy decreased with increasing the shear rate and shear stress, where the value of viscous activation energy reflectes the temperature–sensitivity of real viscosity.

Elastic properties for vaseline were studied by determining the die swell ratio (B) (Barus effet), and it was found that (B) increased with increasing shear stress, but it decreased with increasing L/R ratio, while the temperature do not have any effect on (B). The time residence (t_r) of vaseline in the die was deterimined and studied the relationship between (B) and (t_r).

Note: vaseline does not carry any kind of bacteria, because it is unsuitable medium for their growth

Key words: Rheological propreties, Vaseline, Statical state, Bacterial pollution.

° 60–38

.(Charles Panati, 1998; Yakuji Nippo, LTD., 1984)

.(1987)

(Nishiya, 1993) C¹²-NMR

(Ishiwata, 1997) IR (Nakahara, 1997)

. ° 40

:

(15, 20, 25)°C :

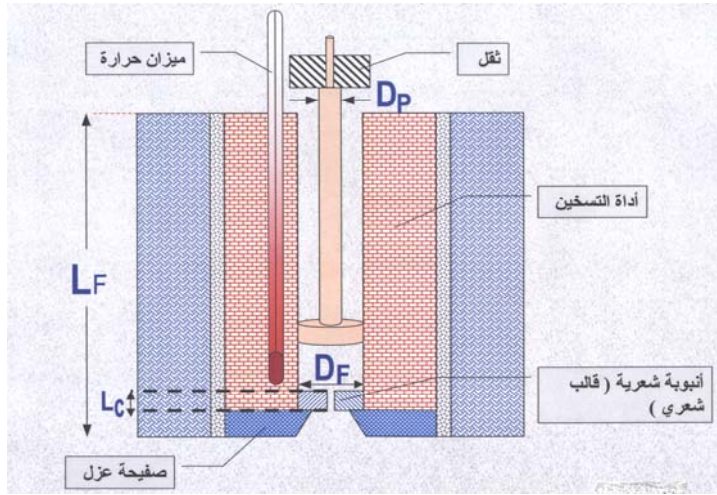
() P_a = (3,24.10⁵ ; 4,68.10⁵ ; 5,76.10⁵)

(1) (Deri, F., *et al.*, 1989)

:(1)

(1)

4	3	2	1	
64	32	16	8	L (mm)
2	2	2	2	D (mm)
64	32	16	8	L/R



(1)

-1

-1-1

:(Deri, F., et al., 1989; Deri, F., 1985)

$$\Delta P_C = \Delta P_a - \frac{\rho \cdot V^2}{\alpha} \quad (1)$$

$$\Delta P_C = \Delta P_a - \frac{\rho \cdot Q^2}{\alpha \cdot \pi^2 \cdot R^4}$$

$$\alpha = \frac{(4n+2)(5n+3)}{3(3n+1)^2} \quad :$$

.(Pa)	-P _a	.(Pa)	-P _C
.(cm/sec)	-V	.	-ρ
.(cm ³ /sec)	-Q	.	-α
.	-n	.(cm)	-R

% 0.01

-2-1

:(Lebianc, J. L., 1974)

$$\Delta P_F \% = \frac{1}{1 + \frac{1}{\frac{L_F}{L_C} \left(\frac{R_C}{R_F} \right)^{3n+1}}} \cdot 100 \quad (2)$$

-ΔP_F

-L_F

-L_C

-R_F

-R_C

-n

% 0.3

τ_c

(e)

-3-1

(1)

(Bagley, E. B., 1961) (Bagley, E. B., 1987)

P_c

(e)

L/R

P_c

(2)

.15°C

$$\tau_c = \frac{P_c}{2 \left(\frac{L}{R} + e \right)} \quad (3)$$

(Pa)

-P_C (dyne/cm²)

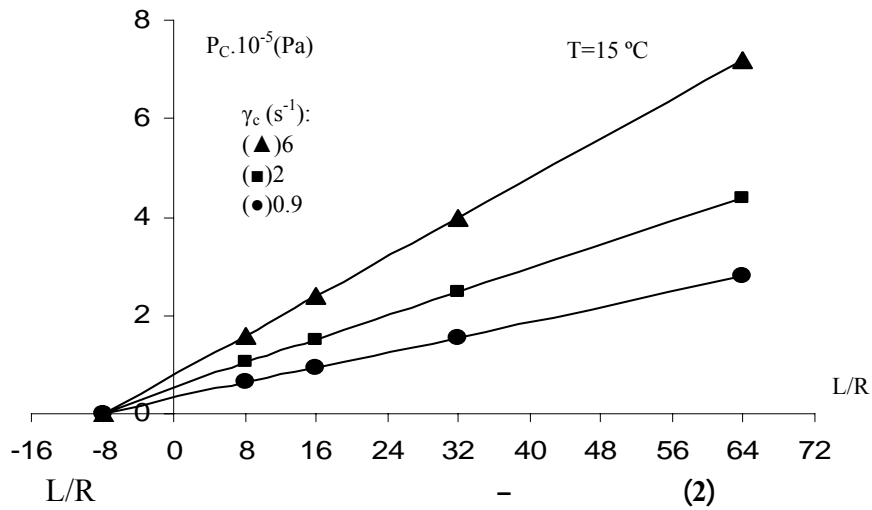
-τ_C

(cm)

-R (cm)

-L

-e



γ_c : -4-1

$$\gamma_c = \frac{(3n+1)}{4n} \cdot \gamma_a \quad (4)$$

$\frac{(3n+1)}{4n} \cdot (\text{sec}^{-1})$: γ_a :

(Mooney, M., 1931; Rabinowitsch, B., 1929)

γ_c

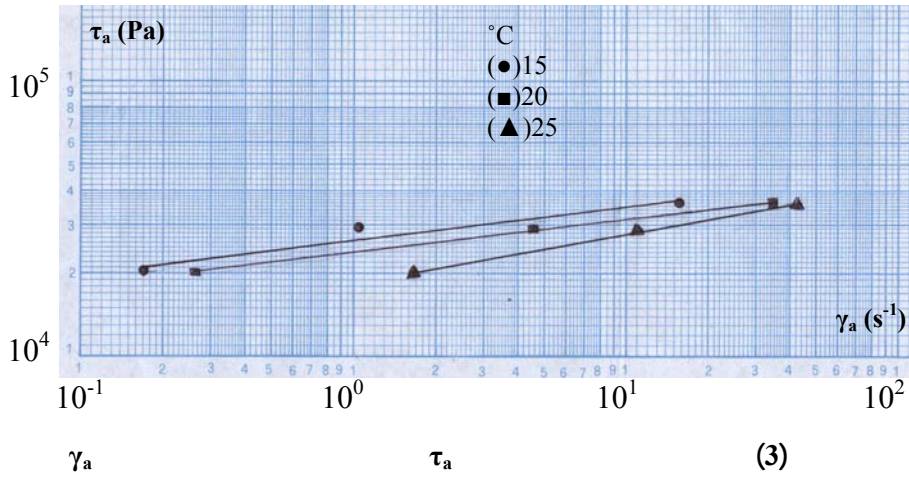
-2

τ_a

(3)

(15, 20, 25)°C

γ_a



n

:

$$n = \frac{d(\log \tau_a)}{d(\log \gamma_a)} \quad (5)$$

n

(n<1)

(Genillon, R., 1980; Deri, F., *et al.*, 1976; Cogswell, F. N., 1981)

:

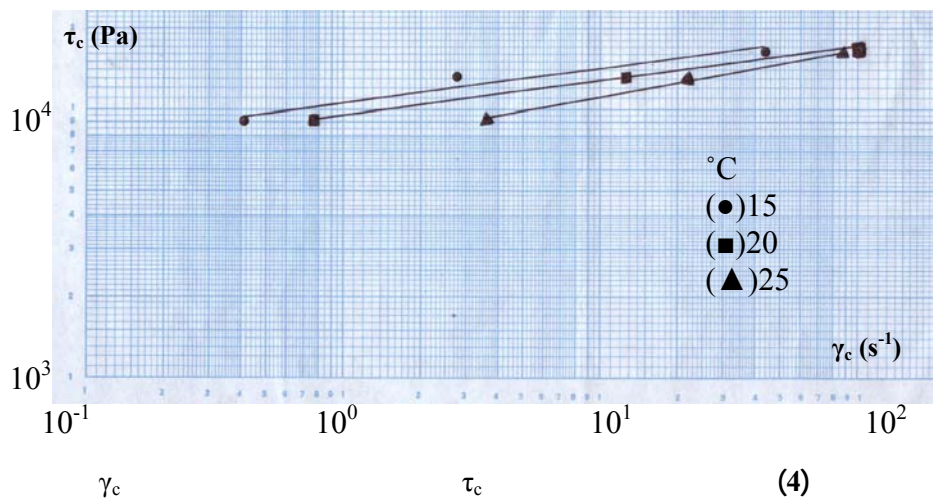
n

(2)

n (2)

25	20	15	(°C)
0.178	0.117	0.123	n

(4)



-3

γ_a

η_a τ_a
:(Deri, F., Genillon, R., 1985)

$$\gamma_a = \frac{4 \cdot Q}{\pi \cdot R^3} \quad (6)$$

:(Deri, F., Genillon, R., 1985)

.(sec⁻¹) τ_a
 .(cm³/sec) Q
 .(cm) R

:(Deri, F., Genillon, R., 1985)

$$\tau_a = \frac{P \cdot R}{2 \cdot L} \quad (7)$$

:(Deri, F., Genillon, R., 1985)

.(Pa) τ_a
 .(Pa) P
 .(cm) R
 .(cm) L

:(Deri, F., Genillon, R., 1985)

$$P = \frac{G \cdot 981}{\pi \cdot R_d^2} \quad (8)$$

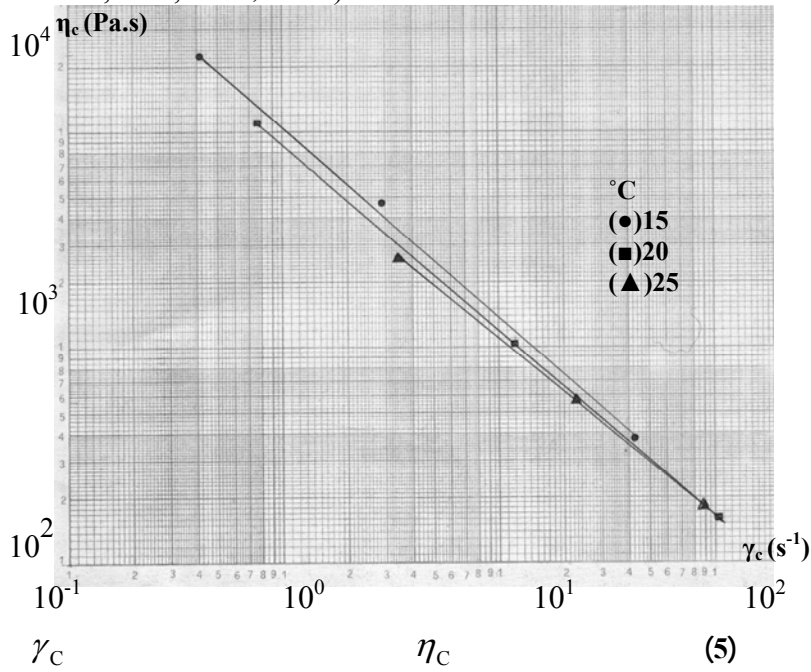
(g) -G (cm) -R_d
-4

γ_c τ_c
:(Deri, F., Genillon, R., 1985) η_c

$$\eta_c = \frac{\tau_c}{\gamma_c} \quad (9)$$

$\cdot \gamma_c$

.(Montfort, J. P., et al., 1978)



(M.F.I)

-5

:(2007)

$$\text{M.F.I} = 600 \cdot \frac{G_m}{t} \quad (10)$$

.(sec)

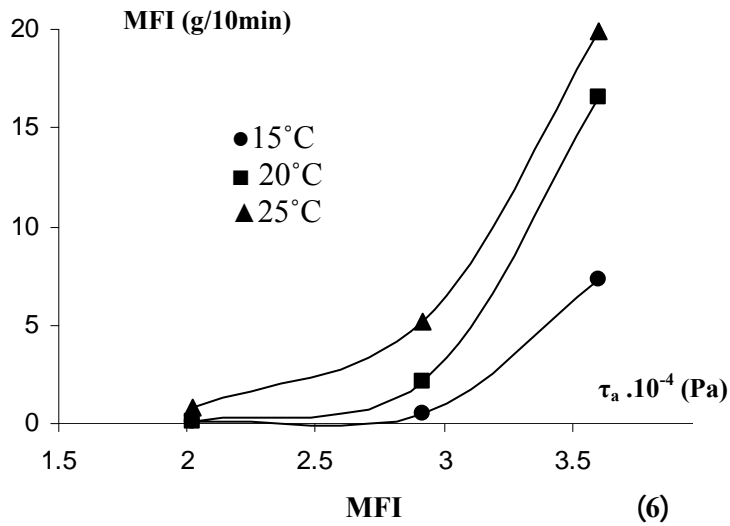
- t .(g)

-G_m

τ_a

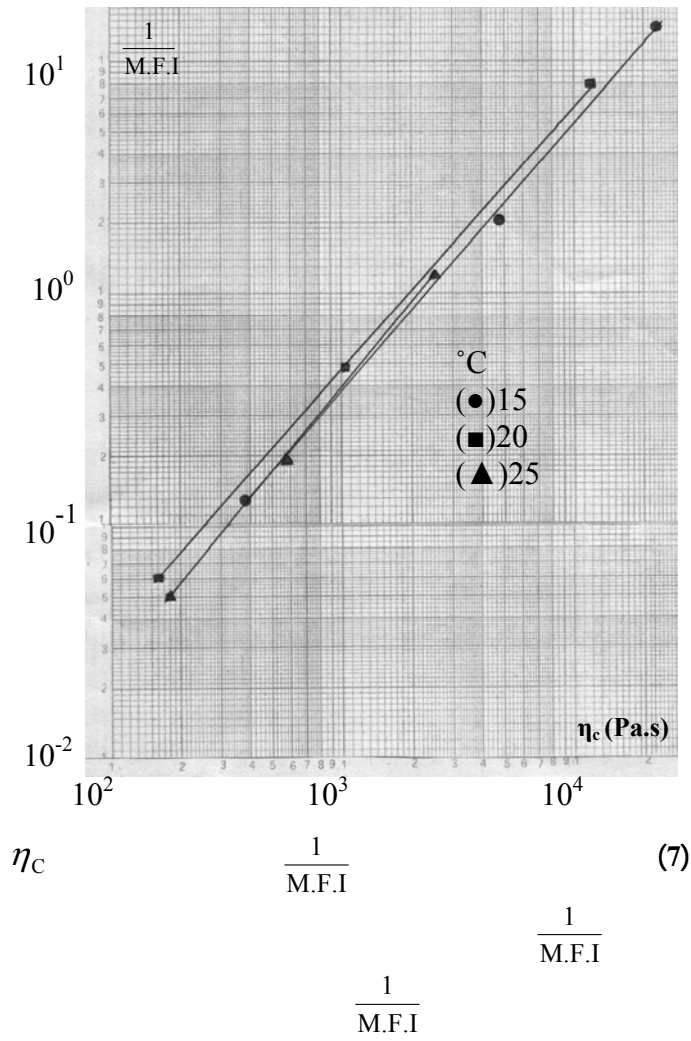
MFI

(6)



$$\frac{1}{\text{M.F.I}}$$

(7)



-6

(Deri, F., *et al.*, 1989; Genillon, R., Derie, F., 1977; Derie, F., 1978; Verry, V., *et al.*, 1981; Muliawan, E. B., Hatzikiriakos, S. G., 2007)

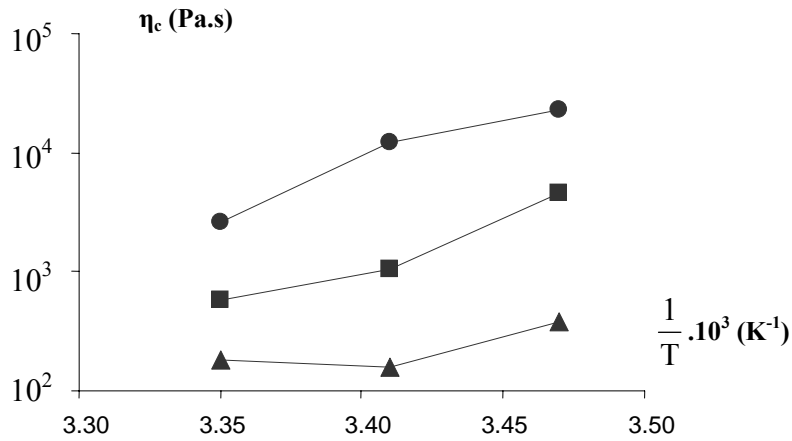
$$\eta_c = A \cdot e^{\frac{E_\tau}{R.T}}$$

$$\eta_c = A \cdot e^{\frac{E_\gamma}{R.T}}$$

$$\ln \eta_c = \ln A + \frac{E}{R.T} \quad (11)$$

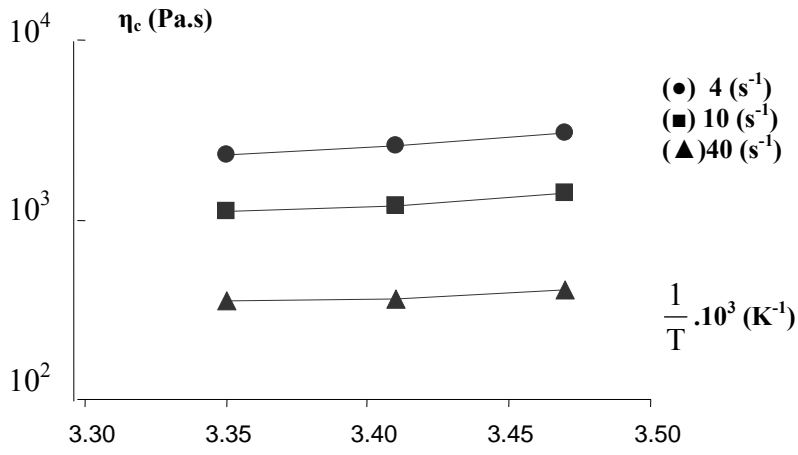
(J/mol) $- E\tau_c$
 (J/mol) $- E\gamma_c$
 (R=8.314 J.mol⁻¹.K⁻¹) $- R$
 (Pa.s) $- \eta_c$ $- A$ (°K) $- T$

(9) (8)



(8)

(●) 9,21.10³ (Pa) (■) 1,33.10⁴ (Pa) (▲) 1,638.10⁴ (Pa)



(9)

(3)

:

E_γ	$E_\tau \text{ (KJ/mol)}$		
$\tau_c \text{ (Pa)}$	$9,21 \cdot 10^3$	$1,33 \cdot 10^4$	$1,638 \cdot 10^4$
$E\tau_c \text{ (KJ/mol)}$	5.03	3.10	1.93
$\gamma_c \text{ (s}^{-1}\text{)}$	4	10	40
$E\gamma_c \text{ (KJ/mol)}$	1.26	0.84	0.24

(3)

(3)

.(Jaziri, M., 1992; Liorens, J., *et al.*, 2003)

-7

.(Genillon, R., Derie, F., 1977)

$$B = \frac{D}{D_0} \quad (12)$$

(cm)

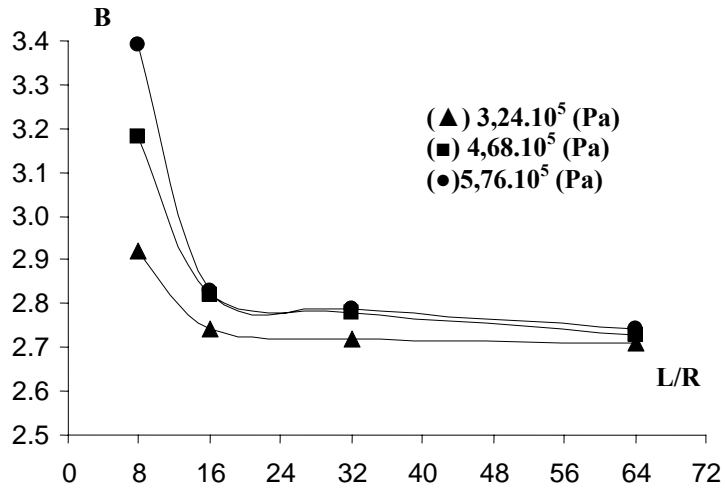
(25)°C

$$\frac{-D}{L/R} = B \quad (10)$$

(cm)

:
- B
-D₀

:P



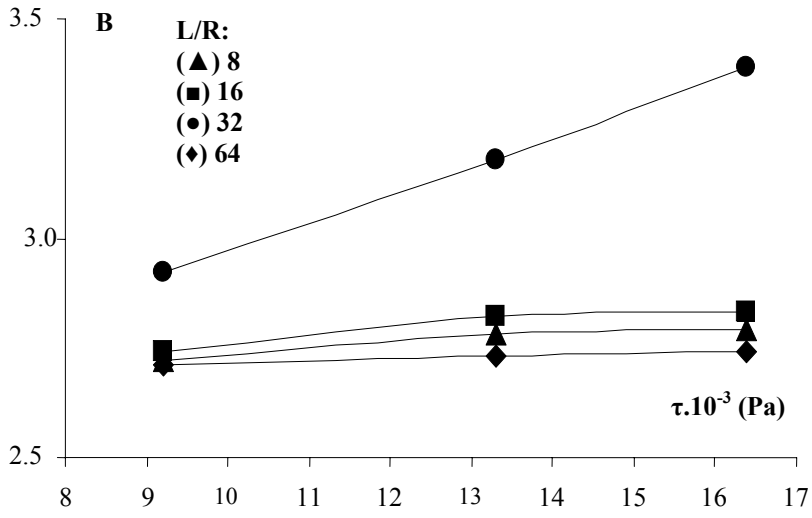
$$\frac{L/R}{B} = B \quad (10)$$

$$B = \frac{L/R}{B} \quad (10)$$

$$L/R$$

B

$$B = \frac{L/R}{B} \quad (11)$$



B (11)

-8

(γ)

L/R
 :(Deri, F., Genillon, R., 1978)

$$t_r = \frac{4 \cdot L}{\gamma_a \cdot R} \quad (13)$$

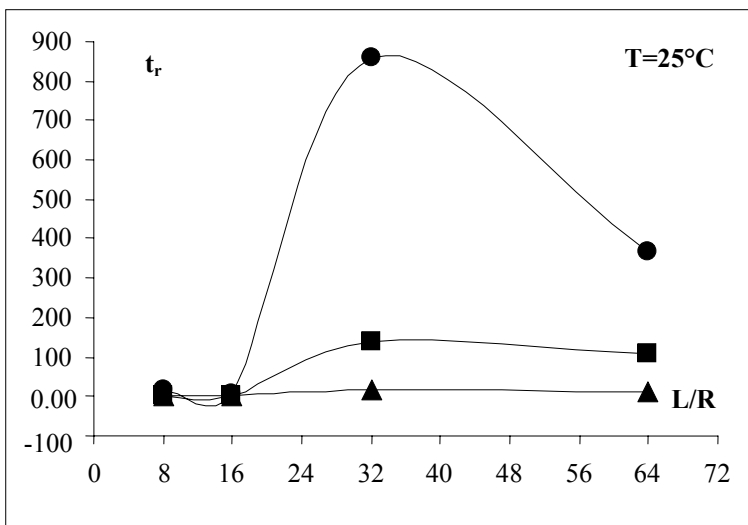
.(cm) -L .(sec) :

.(sec⁻¹) -γ_a .(cm) -t_r

(4) L/R t_r (12) -R

E_γ E_τ (KJ/mol) (3)

γ_a	64	γ_a	32	γ_a	16	γ_a	8	L/R
0.7	365.7	0.1	859.1	9.2	6.9	1.6	19.0	t_r
2.3	109.9	0.9	137	25.1	2.5	10.9	2.9	
21.2	12.1	8.9	14.3	82.8	0.7	42.1	0.7	



L/R t_r (12)

			n	.1
γ_c		η_c	(n<1)	.2
				.3
B				.4
	L/R			.5
		()		

REFERENCES

.1987 .

.2007 .

- Bagley, E. B., 1957. End corrections in the capillary Flow. of Polyethylene, J. Appl. Phys.,V. 28, p. 624
- Bagley, E. B., 1961. Energy of Activation For viscous Flow. Trans. Soc. Rheol.,V. 5, p. 355.
- Charles Panati., 1998. Universalgeschichte der ganz gewöhnlichen Dinge, München S. 282.
- Cogswell, F. N., 1981. Polymer Melt Rheology. London. John Willey.50p.
- Deri, F. Majid, B. Aldiab, F., 1989. Influence de la Temperature sur l'Écoulement des Polymères. Die Angewandte Makromolekulare Chemie, V.173, PP.1-13 (Nr.2581).
- Deri, F., 1985. Etude des Propriétés Rheologiques de Mélanges de Polypropylène – Polystyrène et de Polystyrène-Polyéthylène Basse-Densité . R.J.of Aleppo Univ., No 7 ,pp. 59-78.
- Deri, F. Piloze, R. May J. F., 1976. Etude des Propriétés rhéologiques de quelques mélanges polybuténé -1- polypropène Alétat fondu. Die Angewandte Makromolekulare Chemie,V. 55 , pp.97-108.(Nr.814).
- Deri, F. Genillon, R., 1985. Etude des Propriétés des mélanges de Polypropylène – Polystyrène et de Polystyrène –Polyéthylène Basse-Densité. Die Angewandte Makromolekulare Chemie, V. 134, pp.11-22 (Nr.2092).
- Deri, F., 1978. Etude des Propriétés rhéologiques Alétat fondu de quelques mélanges binaires de Polyéthylène et de Polybutène-1. Thèse de université de pau – France, 120p.
- Deri, F. Genillon, R., 1978. Etude des propriétés rhéologiques des mélanges fondus de Polypropène et de Polybutène -1 à des cisaillements faibles. Die Angewandte Makromolekulare Chemie,V. 68 ,pp. 67- 85 (Nr.1002).
- Genillon, R., 1980. Etude des Propriétés rhéologiques de mélanges de Polypropène et de Polybutene-1 Alétat Fondu Correlation avec leur Mise en oeuvre par Extrusion. The'se Docteur. St. Etienne , 80p.
- Genillon, R. Deri, F., 1977. Etude des Propriétés rhéologiques de mélanges fondus de Polybutène-1 et de Polypropène à des cisaillements élevés . Die Angewandte Makromolekulare Chemie,V. 65 ,pp. 71- 93 (Nr.928).
- Ishiwata Katsumi Shiseido Research Center., 1997. Infrared absorption spectrum measurement operation conditions.

- Jaziri, M., 1992. Etude du greffage Alétat fondu de l' anhydride maléique Sur l' abs. Influence dn compose obtenu. Sur l élaboration et les Propriétés mélanges Polycarbonate/ABS. Thèse Soutenu le 20 v'evrier.
- Lebianc, J. L., 1974. Rheologie Experiment des Polymers Alétat fondu CeBeDoc, Liege, p. 33.
- Liorens, J. Rude, E. Marcos, R. M., 2003. Production of polymolecular Weight distribution from Rheology Polydimethylsiloxane blends, Polymer, V. 44, pp.1741-1750.
- Montfort, J. P. Marin, G. Arman, J. Monge , Ph., 1978. Blending law for binary blends of fractions of linear Polystyrene. Polymer, V. 19, pp. 277-284
- Mooney, M., 1931. melt viscosity of Polyethylene . Rheology, V.2, p. 210.
- Muliawan, E. B. Hatzikiriakos, S. G., 2007. Rheology of Mozzarella Cheese, Interational Dairy Journal, V.17, pp. 1063-1072.
- Nakahara Kazuyoshi Shiseido Research Center., 1997. Gas chromatography operation conditions.
- Nishiya Hiroshi Shiseido Research Center., 1993. ¹²C-nuclear magnetic resonance spectrometry operation conditions,
- Rabinowitsch, B., 1929. End corrections in the capillary Flow of Polymers, Z. Phys. Chem. Abt. A, V.145, p. 1.
- Verry, V. Genillon, R. Niviere, J. May J. F., 1981. Dynamic viscosity of various samples of Polypropene Polyvinylchloride. Rheol. Acta, V. 20, pp.478-483 .
- YAKUJI Nippo, LTD., 1984. The Japanese Standards of Cosmetic Ingredients Second Edition (Annotation) I. pp 1299-1301